

Amendment and Response dated: April 28, 2003 Reply to Office Action of: January 30, 2003

Docket No.: 1085-2 RCE

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## A. Amendments to the Claims:

The below listing of claims will replace all prior versions and listings of claims in the subject application.

Claim 1. (Currently Amended) A process for recovering ethane from a hydrocarbon gas stream having methane, ethane and propane comprising:

providing the hydrocarbon gas stream comprising from about  $40 \underline{50}$  % to about  $80 \underline{75}$  % by mole methane, from about  $10 \underline{15}$  % to about  $10 \underline{40}$  % by mole ethane and from about  $10 \underline{40}$  % by mole propane;

cooling the hydrocarbon gas stream by refrigeration to form a cooled <u>and substantially</u> condensed hydrocarbon <u>feed</u> gas stream, wherein said cooling of said hydrocarbon gas stream by refrigeration does not include turbo-expansion of said hydrocarbon gas stream;

separating the cooled <u>and substantially condensed</u> hydrocarbon <u>feed</u> gas stream into a methane-rich stream and an ethane/propane-rich stream, said methane-rich stream having a first pressure and a first temperature;

expanding said methane-rich stream from said first pressure to a second pressure to lower the temperature of said methane-rich stream from said first temperature to a second temperature to provide a cooling source for said refrigeration, wherein said second pressure is lower than said first pressure and further wherein said second temperature is lower than said first temperature;

separating said ethane/propane-rich stream into an ethane-rich stream and a propane-rich stream; and

recovering said ethane-rich stream.

Claim 2. (Original) The process of claim 1 wherein said expanding of said methanerich stream further includes:

turboexpanding said methane-rich stream.



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Claim 3. (Original) The process of claim 1 wherein said expanding of said methanerich stream further includes:

compressing said methane-rich stream into a compressed methane-rich stream; cooling said compressed methane-rich stream; and turboexpanding the cooled and compressed methane-rich stream.

Claim 4. (Currently Amended) The process of claim 1 wherein separating said cooled and substantially condensed hydrocarbon <u>feed-gas</u> stream further includes:

distilling said cooled <u>and substantially condensed</u> hydrocarbon <u>feed</u> gas stream in a demethanizer column.

Claim 5. (Original) The process of claim 1 wherein separating said ethane/propane-rich stream further includes:

distilling said ethane/propane-rich stream in a de-ethanizer column.

Claim 6. (Canceled)

Claim 7. (Canceled)

Claim 8. (Original) The process of claim 1 wherein said ethane-rich stream contains at least 90 % by mole ethane.

Claim 9. (Original) The process of claim 1 wherein said ethane-rich stream contains at least 96.5 % by mole ethane.

Claim 10. (Original) The process of claim 9 wherein said ethane-rich stream contains less than about 0.5 % by mole methane and less than about 3% by mole propane.



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Claim 11. (Original) The process of claim 1 wherein said methane-rich stream contains at least 95% by mole methane.

Claim 12. (Currently Amended) A process for recovering ethane from a methane, ethane and propane containing gas stream comprising:

providing the hydrocarbon gas stream comprising from about  $40 \underline{50}$  % to about  $80 \underline{75}$  % by mole methane, from about  $10 \underline{15}$  % to about  $10 \underline{40}$  % by mole ethane and from about  $10 \underline{40}$  % by mole propane;

cooling the hydrocarbon gas stream to provide a vapor hydrocarbon feed stream and a condensed liquid hydrocarbon feed stream;

cooling the <u>vapor</u> hydrocarbon gas <u>feed</u> stream in a cryogenic heat exchanger <u>by heat</u> exchange with a first cooling source, a second cooling source and a third cooling source to form a cooled <u>and substantially condensed</u> hydrocarbon <u>feed</u> gas stream, wherein said <u>first</u> cooling is said <u>condensed liquid hydrocarbon feed stream</u> of said hydrocarbon gas stream does not include turbo expansion of said hydrocarbon gas stream;

distilling the cooled <u>and substantially condensed</u> hydrocarbon <u>feed</u> gas stream <u>and the</u> <u>condensed liquid hydrocarbon feed stream</u> in a demethanizer column to form a methane-rich stream and an ethane/propane-rich stream, <u>wherein methane-rich stream is said second cooling source</u>;

compressing said methane-rich stream to form a compressed methane-rich stream; cooling said compressed methane-rich stream to form a compressed methane-rich stream;

turboexpanding said compressed methane-rich stream to a lower pressure to provide a said third cooling source for said cryogenic heat exchanger;

distilling said ethane/propane-rich stream in a de-ethanizer column to form an ethane-rich stream and a propane-rich stream; and

recovering said ethane-rich stream.

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Claim 13. (Original) The process of claim 12 wherein said ethane-rich stream contains at least 96.5 % by mole ethane.

Claim 14. (Currently Amended) A process for providing a methane-rich stream from a hydrocarbon stream containing methane, ethane and propane comprising:

providing the hydrocarbon gas stream comprising from about  $40 \underline{50}$  % to about  $80 \underline{75}$  % by mole methane, from about  $\frac{10}{15}$  % to about  $\frac{50}{40}$  % by mole ethane and from about  $\frac{0.5}{1}$ % to about  $10 \pm 4$  by mole propane;

cooling the hydrocarbon gas stream by refrigeration to form a cooled and substantially condensed hydrocarbon feed gas stream, wherein said cooling of said hydrocarbon gas stream by refrigeration does not include turbo expansion of said hydrocarbon gas stream;

separating the cooled and substantially condensed hydrocarbon feed gas stream into a methane-rich stream and an ethane/propane-rich stream, said methane-rich stream having a first pressure and a first temperature;

expanding said methane-rich stream from said first pressure to a second pressure to lower the temperature of said methane-rich stream from said first temperature to a second temperature to provide a cooling source for said refrigeration, wherein said second pressure is lower than said first pressure and further wherein said second temperature is lower than said first temperature;

recovering said methane-rich stream.

Claim 15. (Original) The process of claim 14 wherein said methane-rich stream contains at least 95 % by mole methane.